

CMP – quo vadis?

**Post use options for
CMP waste**

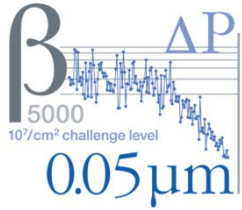
SLS Global Technical Support

The Formula for your SuccessSM

Jochen Ruth

32nd CMP User Meeting
October, 10th, Grenoble

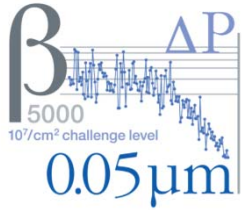
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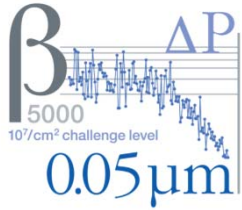
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Content

- Motivation
- General concepts
- CMP wastewater – a valuable resource?
- Prerequisites for re- or downcycling
- State of the art solutions



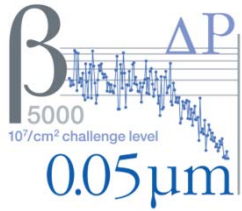
Motivation

CMP, Dicing and Grinding operations

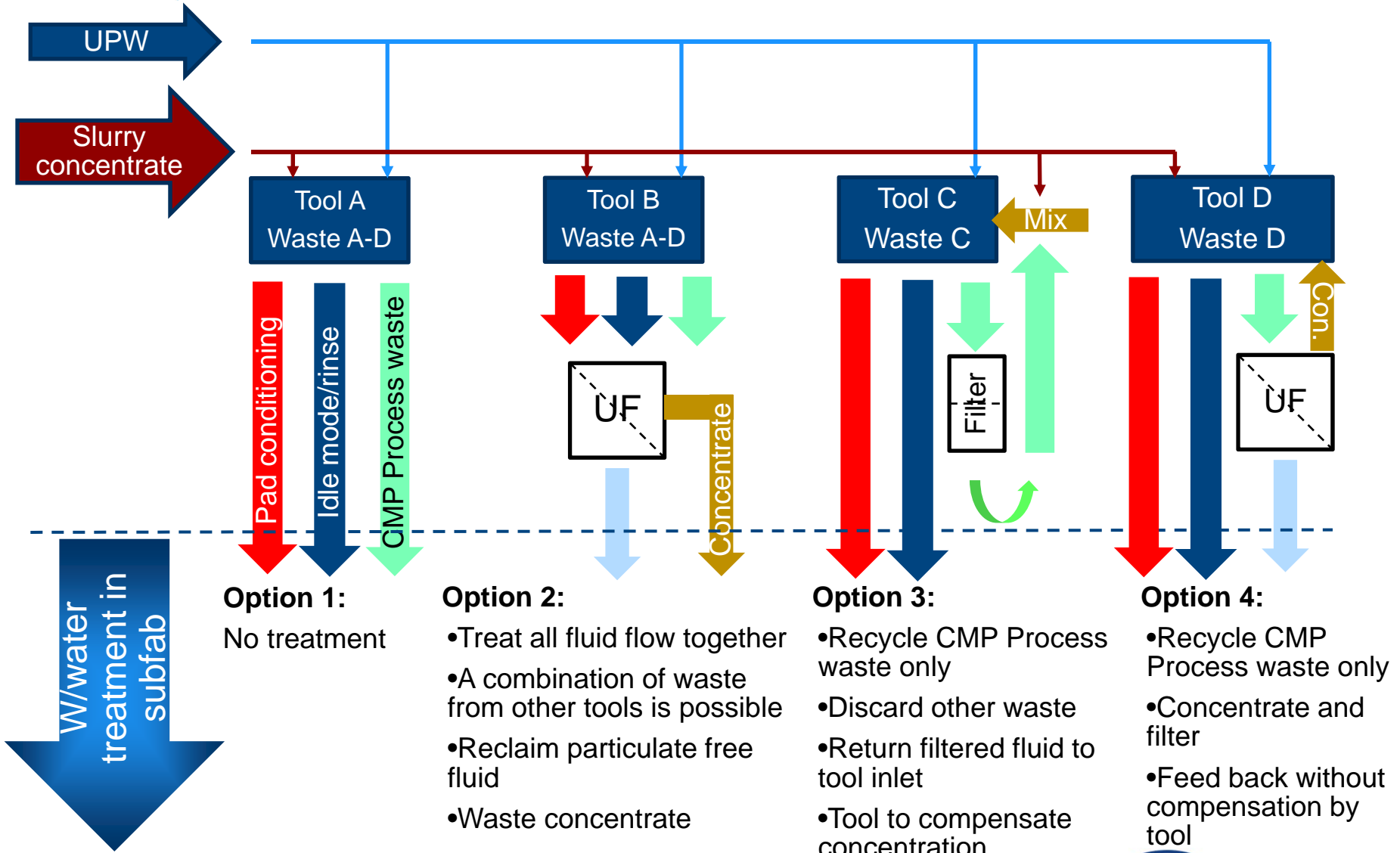
- use very large quantities of high purity water (up to 200 000 m³ per year and site)
- cause large quantities of wastewater containing slurry particles, Si particles, dissolved stabilizers and oxidizers and sometimes heavy metals

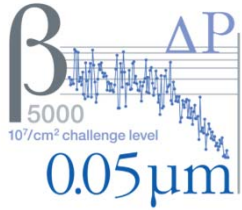
→ Targets for w/water treatment:

- a) Purify w/water to meet discharge limits.... *or*
- b) Water reclaim... *and probably*
- c) Slurry reclaim



Fluid flow schematic for related CMP processes



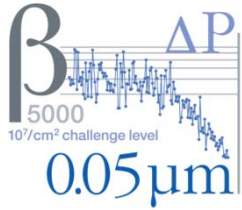


Focus area today: Option 2

- Can be implemented in existing fabs
- Needs minor hardware adjustments
- Provides many options for expansion, upgrade and savings
- Well proven references worldwide
- Very flexible
- Medium to large flow rates preferred

Option 2:

- Treat all fluid flow together
- A combination of waste from other tools is possible
- Reclaim particulate free fluid
- Waste concentrate

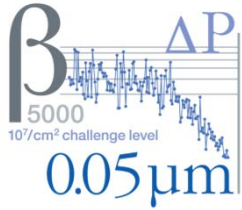


Typical waste water specifications

W/water from	Si Back-grinding	Si Dicing	GaAs Back-grinding	CMP
Suspended Solids	Si	Si	GaAs	SiO ₂ (colloidal or fumed) Al ₂ O ₃ (colloidal or fumed) CeO ₂
TSS mg/l	100...500	10...50	100...500	200...2000
Mean Particle Size/ nm	200	150	200	50...300
pH	6...7	5...7	6...7	3...11
Conductivity μS/cm	< 5	< 5	< 10	< 500
Oxidizers	-	-	-	Fe(NO ₃) ₃ , H ₂ O ₂



W/water may be disposed of after clarification/ neutralization. Reclaim generally possible. Valuable!



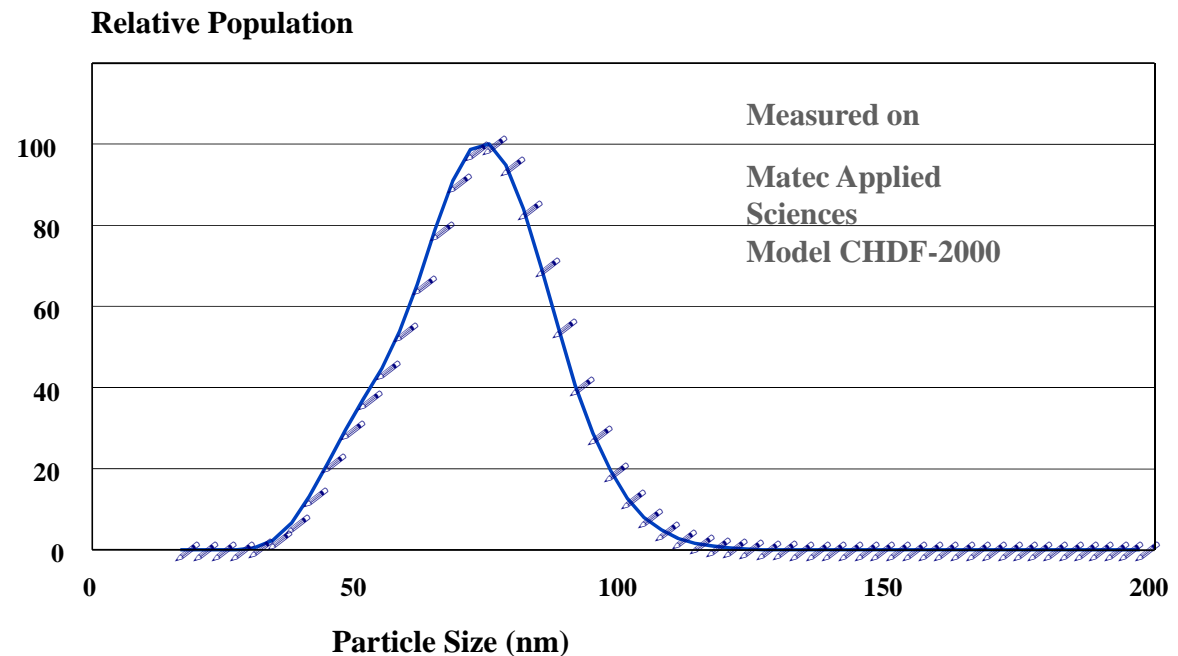
Typical PSD of a CMP Slurry

Example:

Klebosol™ 30N50pHN

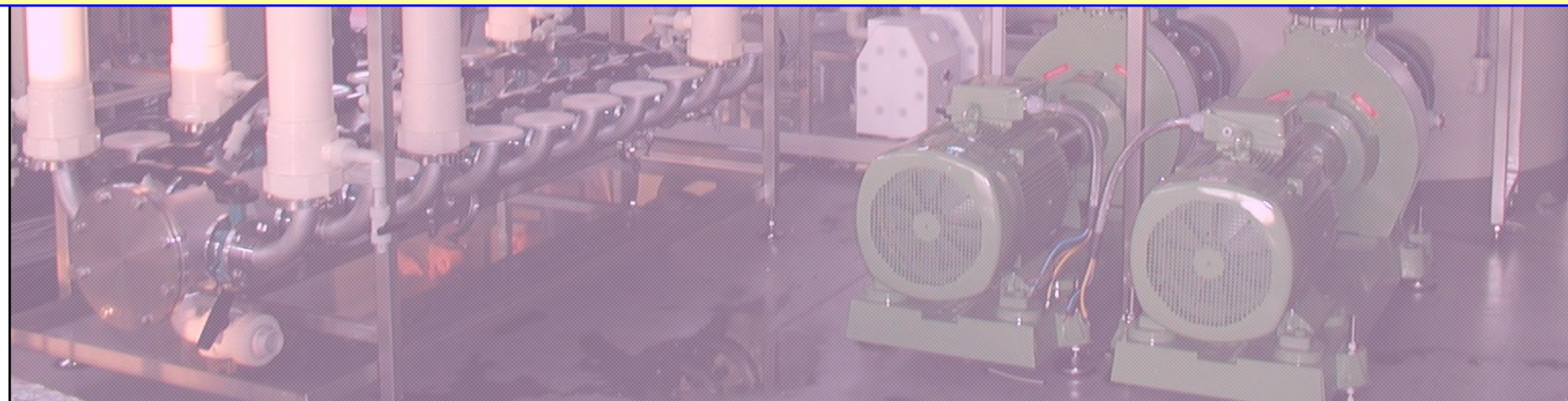
Tendency of Slurry Development:

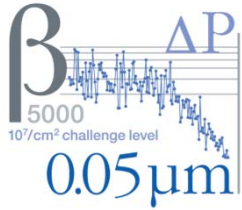
- Smaller particles (down to 10 nm peak size)
- More dilute
- Complex chemistry





Separation of Sub-micron Particles – A Prerequisite for Economical Disposal and Reclaim of Wastewater from Polishing, Grinding and Dicing Operations





Conventional Process to remove sub-micron particles:

Three process steps

1. Destabilization through pH shift and by addition of inorganic coagulants (e.g. ferric or aluminum salts)
 - Coagulation generates small aggregates, sometimes simultaneous precipitation of dissolved matter
2. Agglomeration by addition of polymeric flocculents (e.g. polyacrylates)
 - Formation of large, stable agglomerates
3. Concentration of agglomerates by sedimentation or crossflow microfiltration, followed by sludge dewatering through filters or centrifuges

Principles of W/water treatment

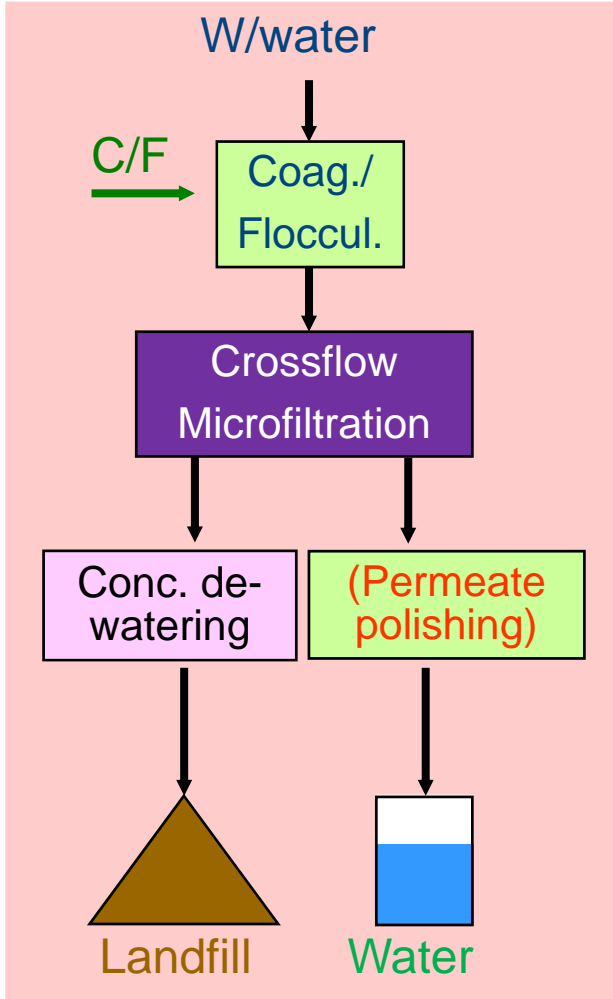
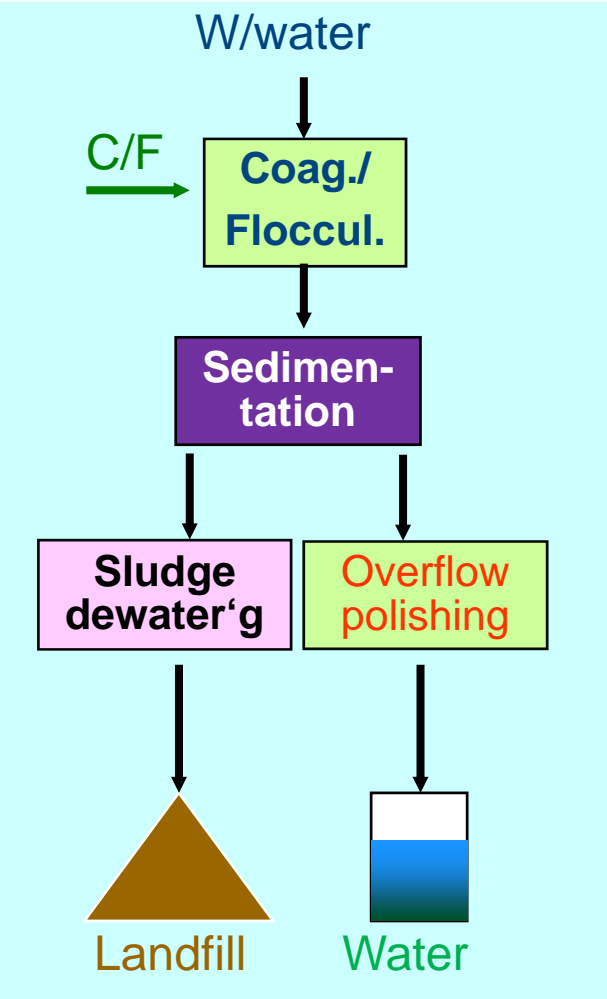
1) Coagulation/ Flocculation/ Sedimentation

(large consumption of chemicals, space and landfill area, rather poor water quality)

2) Coagulation/ Flocculation/ Xflow Microfiltration

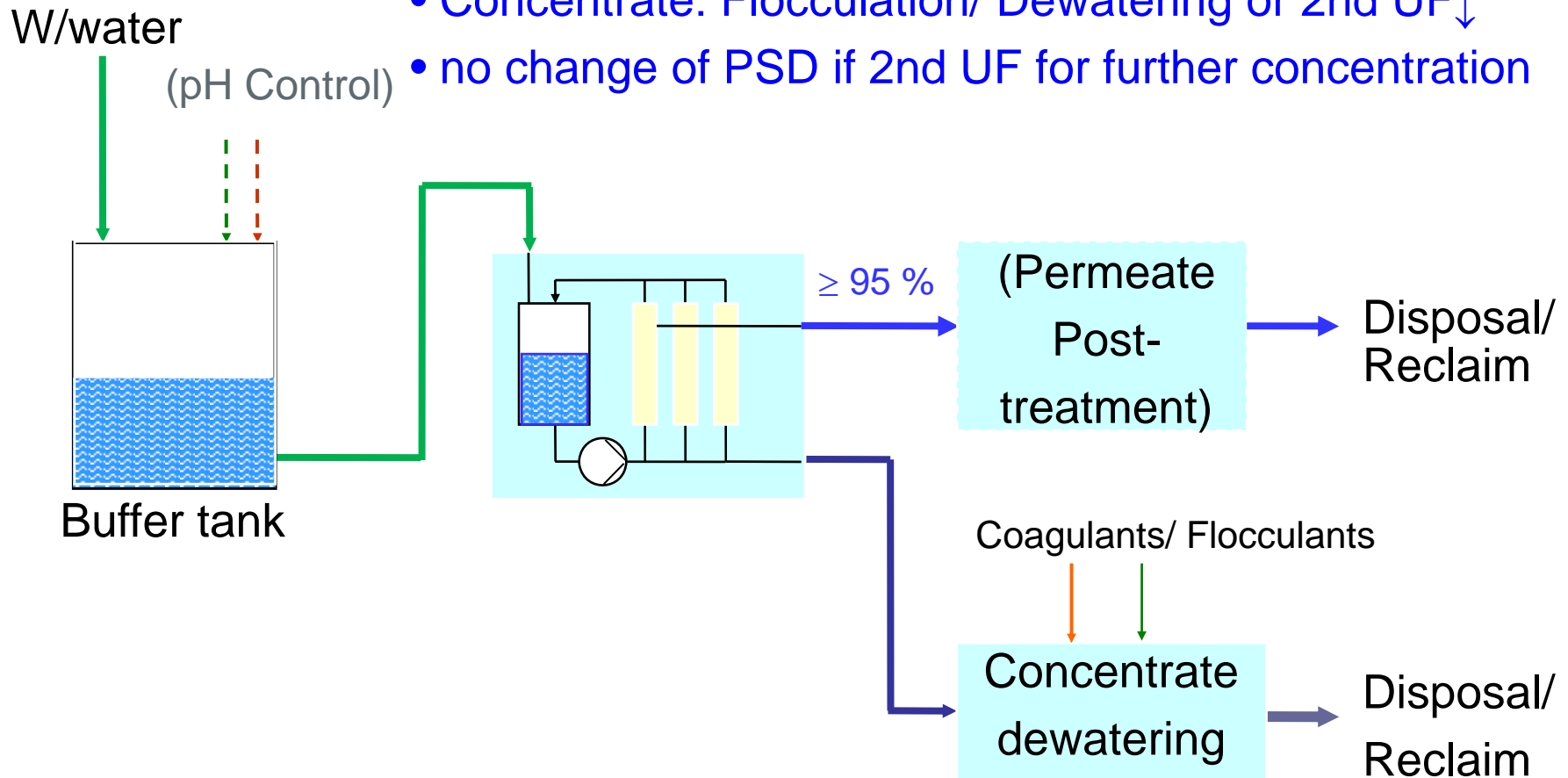
(large consumption of chemicals, space and landfill area, fairly good water quality)

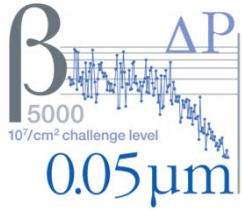
Flocculation of the full feed stream is generally necessary in case of conventional MF membranes!



Solution 3: Direct Ultrafiltration

- Water is not polluted by coagulants/ flocculants
- Permeate Post-treatment: easy by RO, EDI, IEx...
- Concentrate: Flocculation/ Dewatering or 2nd UF↓
- no change of PSD if 2nd UF for further concentration





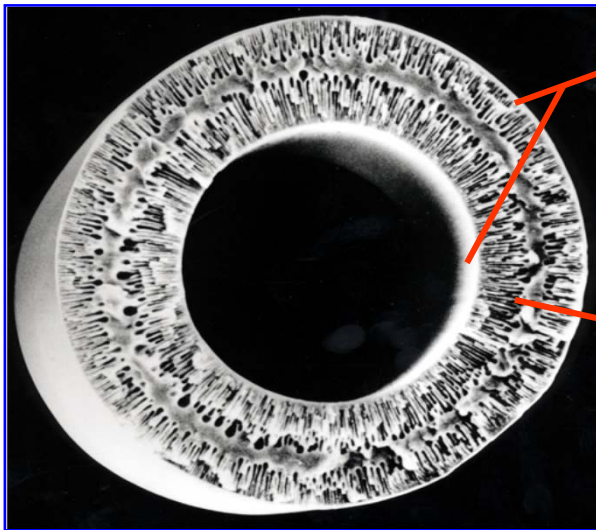
Pall Technology for CMP W/water

- Membranes: - polymeric hollow fibers (PAN, PE, PVDF, depending on w/water spec)
 - ceramic multi-channel elements for special cases
- Process: - Continuous Fed-Batch, inside-out
- References: - 14 systems in Europe, among them 3 sold to end users and 11 to system integrators
- Capacities: - 1 m³/hr to 30 m³/hr (majority > 10 m³/hr)

The removal of particles < 100 nm needs UF membranes with ~ 10 nm pore size



Asymmetrical membrane structure helps to avoid uneconomically large membrane resistance:



Pall Microza[®]

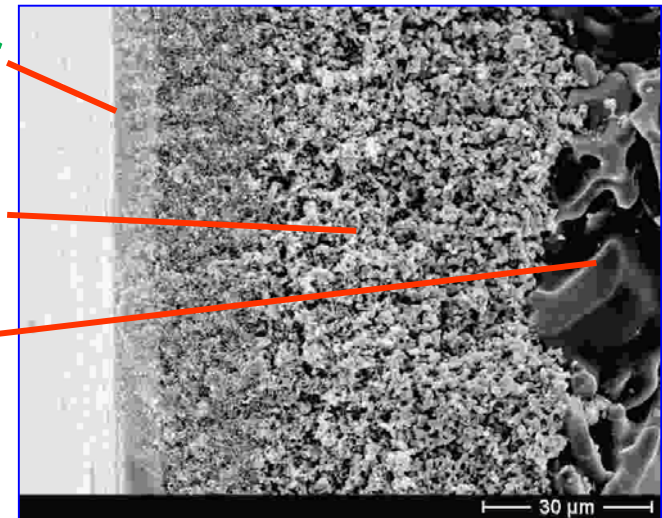
UF hollow fiber membrane (PAN)

active membr. layer

transition

layers

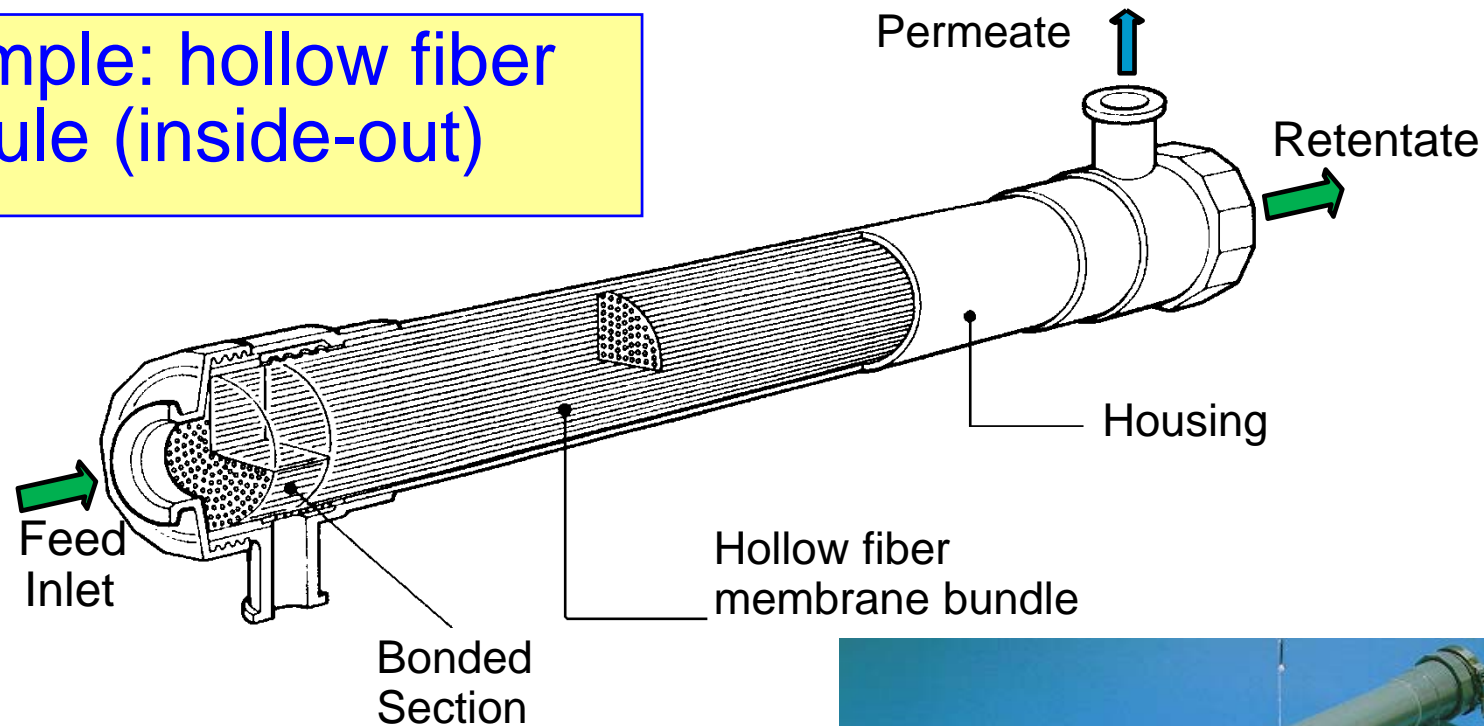
support structure



Pall SCHUMASIV[®]

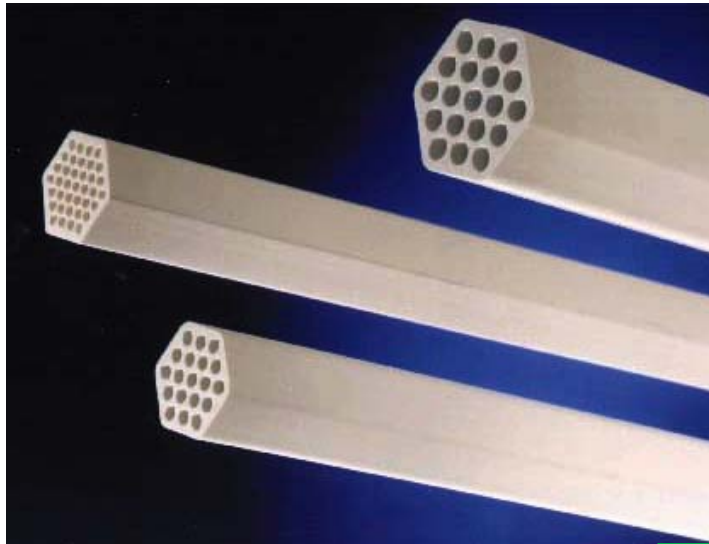
UF ceramic membrane

Example: hollow fiber module (inside-out)



- various housing materials and housing styles (industrial, sanitary)
- several membrane grades, geometries and membrane materials
- membrane area 0.01...12.3 m²



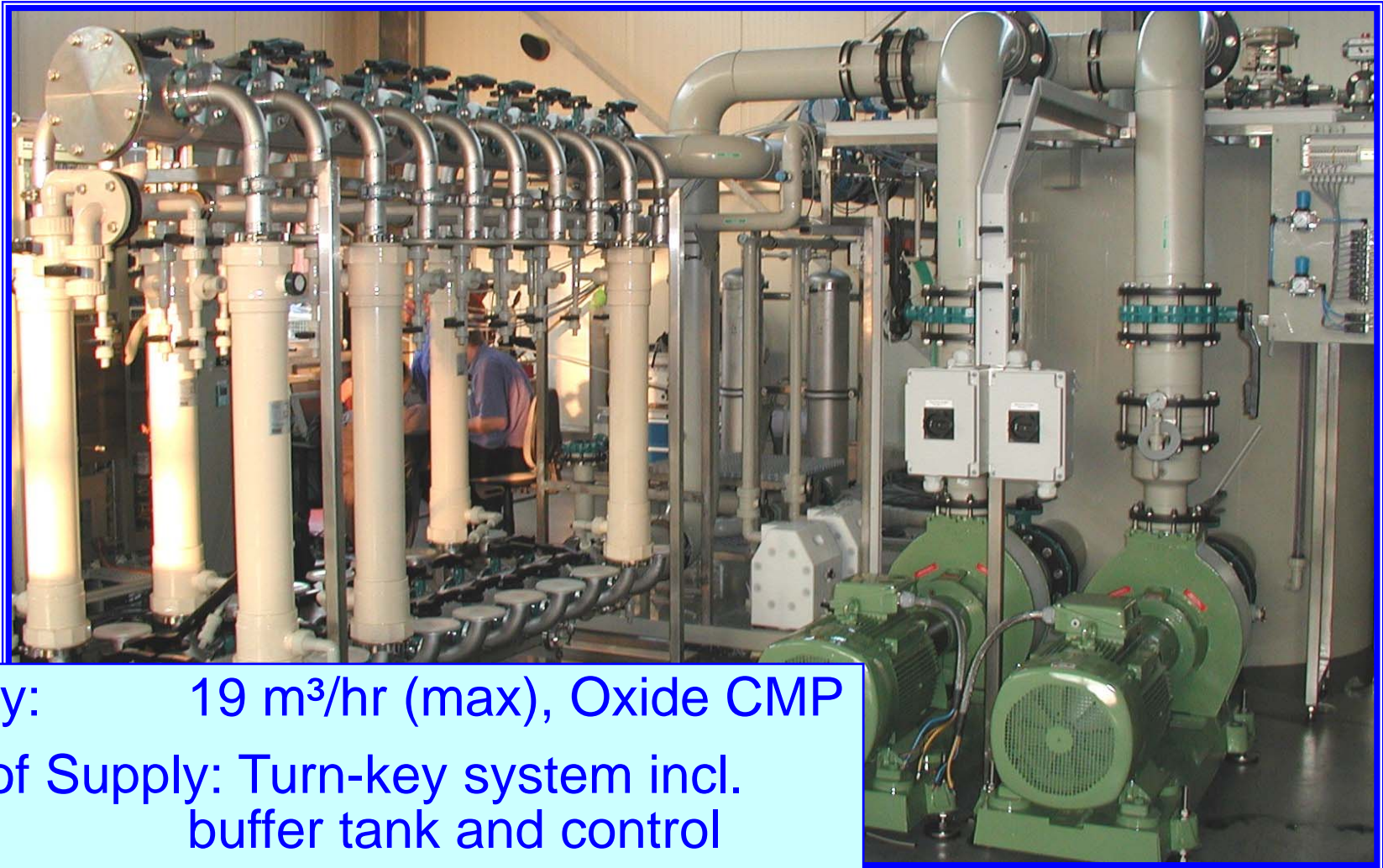


Example: Ceramic elements/ modules

- various housing materials and housing styles (industrial, sanitary)
- several membrane grades, geometries and membrane materials
- membrane area 0.2...21 m²

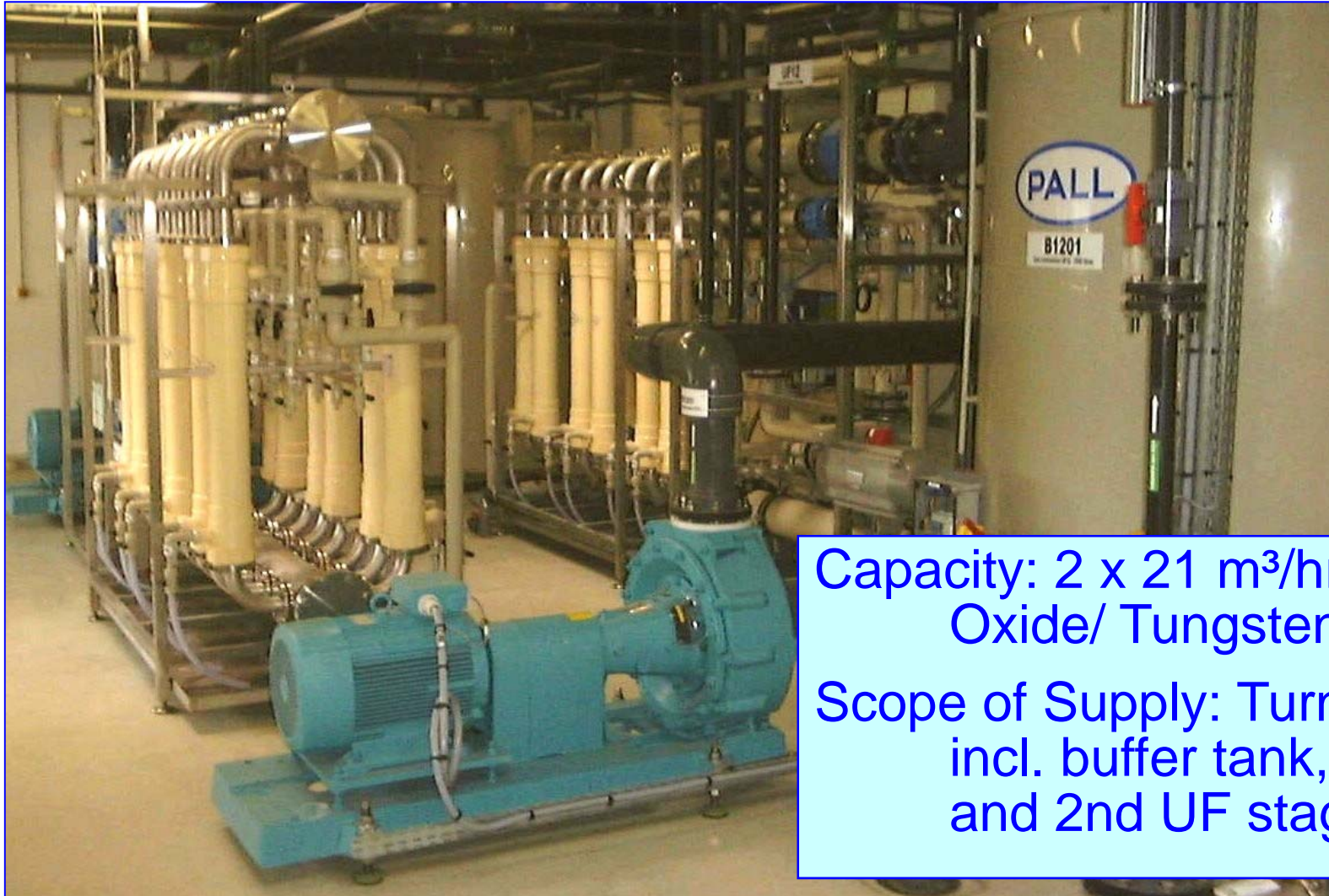


Example 1: German fab System



Capacity: 19 m³/hr (max), Oxide CMP
Scope of Supply: Turn-key system incl.
buffer tank and control

Example 2: French fab system



Capacity: 2 x 21 m³/hr (max),
Oxide/ Tungsten-CMP

Scope of Supply: Turn-key,
incl. buffer tank, control
and 2nd UF stage

Example 3: Concentrate stage CMP



2nd stage

Capacity: 1 m³/hr concentrate
from 1st stage

Final TSS: 350 g/l (equal to
original slurry)

Scope of Supply: Turn-key
system, incl. buffer tank
and control

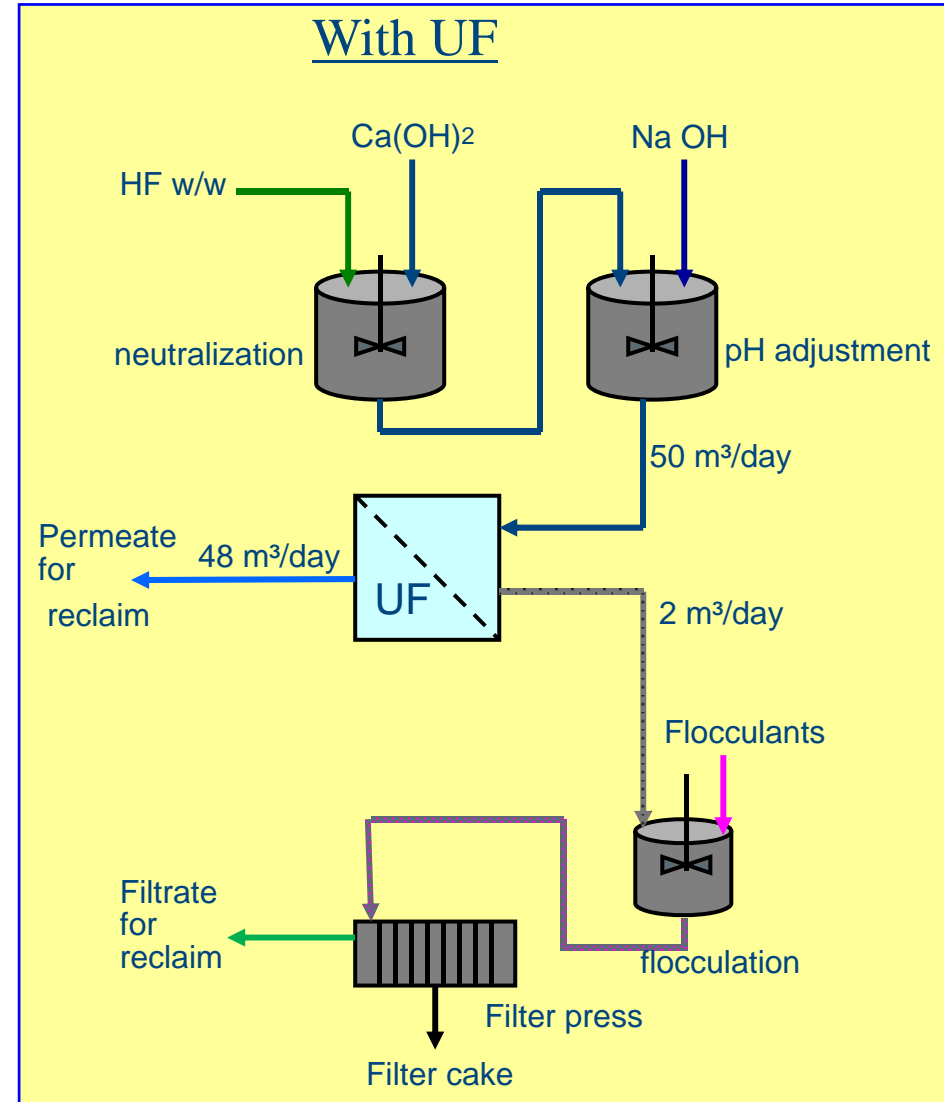
Special: On-line measurement/
control of TSS

Comparison conventional vs UF

- Lower space requirements
- Improved water quality for reclaim
- Reduced consumption of coagulants/ flocculants

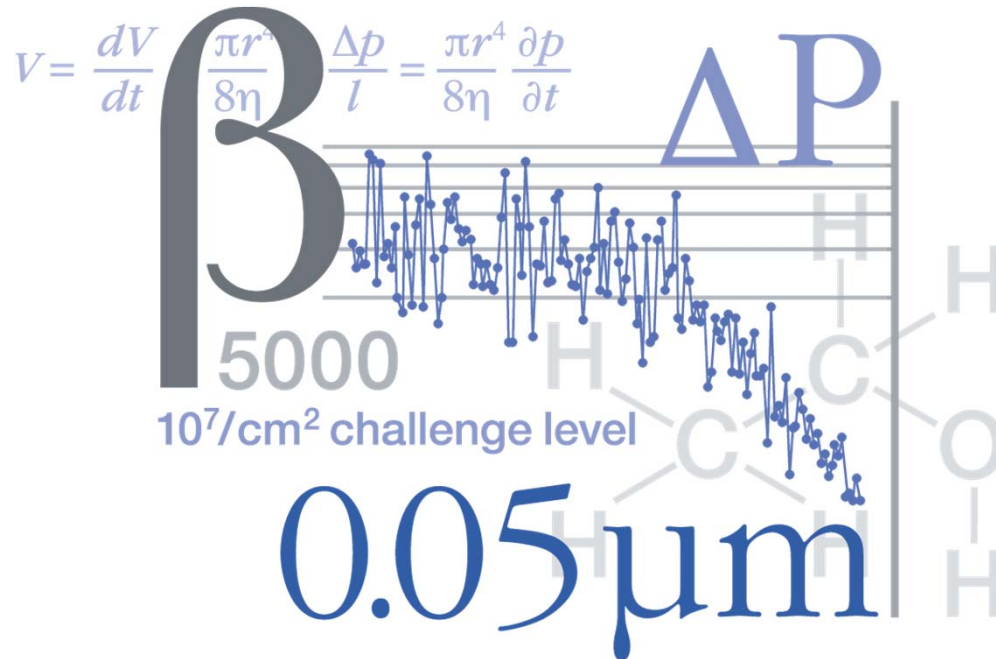
Application e.g.

- For capacity increase of existing treatment systems
- For new systems with space limitations



We are looking forward to our
co-operation...





Pall SLS

A global customer support organization

SLS Global Technical Support

The Formula for your SuccessSM

Jochen Ruth
SLS Director CE

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